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transactions and communications

An evaluation of the falling rod viscometer and the Inkometer for the testing of news inks

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Summary

A Laray falling cylinder viscometer and an Inkometer have been evaluated as ink test instruments using a series of 19 inks carefully formulated to cover the entire range of composition of North American news inks. These inks were also studied using a researchgrade laboratory rheometer, and the results were compared with the data obtained using the two testers.

The ranking of the inks according to high shear viscosity, as determined using the research rheometer, was the same as that based on Laray viscosity at high load, suggesting that the Laray viscometer gives reliable viscosity values. The Inkometer number was found to be a function of time, and the ranking of the inks according to equilibrium value was roughly similar, but not identical, to that based on the high shear viscosity. The Inkometer does not measure any well-defined physical property of an ink.

Introduction

The objective in carrying out ink flow tests is to predict the performance of an ink in the printing press. The correlation of test results with behaviour in the press is not a straightforward matter for several reasons. Firstly, carbon black inks are rheologically complex fluids, and no single type of measurement can provide a complete picture of their flow behaviour. Secondly, there is a lack a fundamental understanding of the detailed nature of the physical processes that occur when an ink film splits at the exit of the printing nip. As a result, it cannot be said with certainty which physical or chemical properties of the ink and substrates govern the ink's behaviour in this process.

There are two approaches to the question of rating inks on the basis of laboratory measurements. One approach is to make a hypothesis about what fluid properties are important and to make an accurate measurement of these properties. The second approach is to use a test procedure that simulates, in some sense, the printing process. Such a procedure does not yield a well-defined physical property but rather an empirical index of ink quality. In this case, the key questions have to do with the reproducibility of the test and its relevance to ink performance in a press.

This paper presents the results of an extensive evaluation of two commercial ink testers, the falling rod viscometer and the Inkometer. The inks used in the study were also subjected to a rheological characterization using an accurate research-grade rotational rheometer.

Experimental

Formulation of test inks

The principal components of a news ink are: pigment, vehicle, a vehicle property enhancing additive (resin in our studies), and an additive to enhance pigment properties (pitch in our studies). The inks used in the present study were prepared by mixing these four ingredients in various proportions. The specific components used are listed below.

- 1. Pigment: Fluffy Elflex 8. A furnace carbon black pigment produced from the middle of a production run to assure a high degree of homogeneity. Manufactured by the €abot Corporation.
- Vehicle: Sunthene 4240 oil. This is a refined version of a commercial news ink carrier liquid.
- Resin: Pico 6140-3. A synthetic hydrocarbon resin made by Hercules.
- 4. Pitch: Pioneer 26 asphaltum pitch. A dispersant made by Witco Chemicals.

The test inks were prepared in the Montreal plant of Canada Printing Ink using standard ink manufacturing techniques. The ink preparation was performed in two stages. The first stage involved the mixing of two "base" liquids, the "black base" and the "varnish". The black base was a 33.33 per cent (by weight) suspension of carbon black in oil, while the varnish was a 30 per cent resin solution in oil. One kilogram ink samples resulted from combining appropriate proportions of the two base liquids with additional oil and asphaltum pitch, as required. The inks were dispersed thoroughly on a triple roll mill.

The compositions were the same as those used in an extensive rheological study, the results of which have been published previously^{1,2} and these are listed in Table 1. These composi-

Table 1
Compositions of model inks
Concentrations in weight per cent)

Ink Number	x ₁ Carbon Black	X2 Oil	Resin	x ₄ Pitch
1	8	92	0	0
2	8	82	10	0
3	8	72	20	0
4	8	80	10	2
5	8	88	0	4
6	8	78	10	4
7	8	68	20	4
8	14	76	10	0
9	14	84	0	2
10	14	74	10	2
11	14	64	20	2
12	14	72	10	4
13	20	80	0	0
14	20	70	10	0
15	20	60	20	0
16	20	68	10	2
17	20	76	0	4
18	20	66	10	4
19	20	56	20	4

tions were selected using established techniques for the design of experiments to cover the entire range of composition of North American news inks, as determined from the listings of the National Association of Printing Ink Manufacturers³.

The densities of the model inks were determined by use of ASTM Standard Test Method D 1475. In addition to the inks, the densities of several resin solutions and the 4240 Sunthene oil were also measured. Through the use of multiple regression, it was found that a linear equation could adequately represent the experimental results.

$$\rho$$
 (Kg/m³) = 934.6 + 4.0615 x₁ + 1.4836 x₃ + 1.2217 x₄

Where

 x_1 = Carbon black (wt per cent) x_3 = Resin (wt per cent) x_4 = Pitch (wt per cent)

The densities of the components were as follows:

Oil: 934.6 Kg/m³ (measured) Resin: 1083.0 Kg/m³ (measured) Pitch: 1056.8 Kg/m³ (inferred from ink densities) Carbon black: 1340.8 Kg/m³ (inferred from ink densities)

Rheological properties of the inks

The basic rheological studies were carried out on a Rheometrics Mechanical Spectrometer (RMS), model 605, equipped with a sensitive torque and normal force transducer (Model T-100). The sample was placed between cone-and-plate fixtures having a diameter of 50 mm and a cone angle of 0.040 radian. The cone apex was ground flat reducing the total cone height by 50.0 μ m. Great care was taken to ensure the precise setting of the gap and alignment of the fixtures. The temperature at which the experiments were conducted was 30 \pm 0.5 °C, which is typical of the temperatures at which printing and ink preparation are carried out. Special shock absorbing pads were placed at the base of the RMS in order to minimize the effects of external vibrations on the T-100 transducer signal.

The Mechanical Spectrometer is a sophisticated, general purpose, rotational rheometer capable of generating a wide range of shearing deformations, including steady shear, oscillatory shear and sudden starting and stopping of shear. The inks used in this study were subjected to extensive testing in the RMS, and the results are discussed in detail elsewhere^{1,2}. We present here a summary of the observations made in this study.

When ink flows through a printing nip, it experiences a complex, time-varying deformation pattern in which the shear rate passes through sharp peaks and even changes its sign. The response of an ink to transient shearing deformations is thus of crucial importance in the printing process. The inks were therefore subjected to a variety of shearing patterns including sudden start-up of shear, interrupted shear and reversal of direction of shear. The results showed that the inks, especially those with significant carbon black content, exhibited complex time-dependent behaviour, being thixotropic and viscoelastic.

In order to establish a quantitative ranking of the inks based on rheological behaviour, they were also subjected to steady shearing to determine the steady state shear stress. Curves of shear stress and viscosity for three typical inks, as functions of shear rate, are shown in figures 1 and 2. All of these inks had a resin content of 9.9 per cent.

In qualitative terms, the inks display shear-thinning behaviour while appearing to have a yield stress. The addition of pitch tends to decrease considerably the ink viscosity at low



Figure 1. Shear stress versus shear rate: □ Ink no. 6; △ Ink no. 8; ◇ Ink no. 14



Figure 2. Viscosity as a function of shear rate: \Box Ink no. 6; Δ Ink no. 8; \Diamond Ink no. 14

shear rates, and the results indicate that there is a definite interaction between pitch and resin. As expected, the viscosity rises with increasing carbon black content. As the shear rate increases, the viscosity appears to approach a limiting value, $\eta_{\rm c}$. This limiting value increases with both resin and carbon black concentration.

The inks were all shear thinning and appeared to have a yield stress. Previous studies of ink rheology^{4,5} have made use of several equations to relate the equilibrium shear stress to the shear rate. These include the Bingham equation and Casson's equation, shown below as equations 1 and 2 respectively.

Where

Where Kc and Ko are constants for a given material.

While Equation 1 is purely empirical, Equation 2 is based on a physical model for a dilute suspension⁶. However, it has been pointed out^{7,8} that Equation 2 has several serious weaknesses, especially in the case of non-dilute suspensions.

We were able to achieve a better fit of our data by use of γ Equation 3

$$\sigma = \sigma_{\rm B} + \eta_{\infty} \dot{\gamma} - \sigma_{\rm L} \exp(-\lambda \dot{\gamma}) \quad \dots \quad \dots \quad \dots \quad \dots \quad (3)$$



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Figure 3. Principal features of the Laray viscometer

The equilibrium shear stress is assumed to be made up of a difference of two contributions. The first follows the classical Bingham fluid behaviour, with a constant slope η_{α} that models the actual ink viscosity at high shear rate, and an intercept σ_{B} , which is greater than the actual yield stress σ_o . The difference between σ_B and σ_o is termed the "stress loss", σ_L . A similar model has been proposed earlier by Shangraw9.

The second response results from the exponential decrease of the stress loss σ_1 with shear rate. The shear rate above which the exponential decrease no longer contributes to the stress is termed the critical shear rate, $\dot{\gamma}_{crit}$, defined as 5/ λ . By substituting:

$$\sigma = \sigma_{\rm L} + \sigma_{\rm o}$$

Equation 3 can be rewritten as:

We have called this the "Bingham Exponential Decrease" (BED) model, since it combines Bingham plastic behaviour with shear rate dependent exponential decrease of the shear stress. Values for the four parameters σ_B , η_{α} , σ_L and λ_1 are listed in Table 2 for seventeen ink formulations.

It is important to note that rotational rheometers are limited to use at rather low shear rates because of the occurrence of flow irregularities at high shear rates. Since the shear rates that an ink experiences in a printing nip are generally much higher than those attainable in a rotational rheometer, it would appear that such a device is of limited usefulness for characterizing inks. However, if confidence could be developed in the general validity of a relationship such as Equation 4 then the results of low shear rate tests could be used to predict the behaviour of the ink at higher shear rates.

Evaluation of the falling rod viscometer

Falling rod viscometers have been used for many years for the industrial testing of fluids, especially for printing inks. Commercial models are available from several manufacturers; the

5	Table 2
Density	measurements

Grouping Number According to		Density at 30°C			
Carbon Black Content	Carbon Black	rbon Oil ack	Resin	Pitch	(kg/m ⁻)
	\mathbf{x}_1	x 2	x ₃	x ₄	
1	8	92	0	0	966.7
. 2	8	82.1	9.9	0	986.6*
				985.1	
4	8	80.1	9.9	2	982.1
5	8	88	0	4	970.8* 972.7
6	8	78.1	9.9	4	986.7
7	8	67.9	20.1	4	1001.8
8	14	76.1	9.9	0	1004.1
9	14	84	0	2	998.3* 997.2
10	14	74.1	9.9	2	1002.6* 1004.9
12	14	72.1	9.9	4	1012.9
16	20	68.1	9.9	2	1031.0* 1032.6
17	20	76	0	4	1015.8
18	20	66.1	9.9	4	1038.9
19	20	55.9	20.1	4	1053.9
Sunthene 4240	0	100	0	0	935.1†
Varnishes	0	90.1	9.9	0	946.25
	0	85.03	14.97	0	959.35
	0	79.9	20.1	0	962.1

Replicate

 $\dagger \rho_{4240 \text{ oil}} = 942.2 \text{ Kg/m}^3, 15^{\circ}\text{C}, \text{ Table 5.7}$

one used in this study was a Laray Viscometer, model VM.01, manufactured in France by Adamel Lhomargy. The principal advantages of this type of viscometer are that it is inexpensive and easy to use and that high shear rates can be generated. The disadvantages are that the temperature is not well controlled and the fluid in the shearing gap is not subjected to a uniform time of shearing.

The basic geometry of the Laray viscometer used in this study is shown in Figure 3, while the important dimensions are:

R.	= 6.00 mm	l
₹,	= 6.03 mm	1
R.,	= 9.33 mm	l
L	= 27.67 mm	i
Lo	= 30.97 mm	l
Н	= 10.0 cm	
α	= 450	

The theoretical equations for calculating the shear rate, shear stress and viscosity for sliding cylinder flow are given in standard reference books on viscometry^{10,11}. The shear stress at the inner wall, σ_1 , is given by Equation 5.

Where

F = Force driving the rod

= Length of the shearing zone L

R₁ = Radius of the rod

Clearly, the independent variable in a falling cylinder viscometer is the shear stress rather than the shear rate. For a Newtonian fluid, the shear rate at the surface of the rod is given by Equation 6.

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$$\dot{\gamma} = \frac{V}{R_1 \ln(R_2/R_1)} \quad \dots \quad \dots \quad \dots \quad \dots \quad \dots \quad \dots \quad (6)$$

Thus, the viscosity of a Newtonian fluid is given by Equation 7.

In addition to the assumption that the fluid is Newtonian, other assumptions made in deriving equations 6 and 7 are:

- 1. The rod and the outer cylinder are coaxial.
- 2. There are no end effects.
- 3. The velocity is constant during the test.
- 4. The temperature is uniform in the fluid.

In the case of the falling rod viscometer, the driving force is provided by gravity acting on the rod together with any weight attached to it. Thus, if M is the total mass of the rod and attached weights,

$$F = Mg$$

If the fluid of interest is not Newtonian, equations 5 and 6 are no longer valid. If an equation relating the viscosity to the shear rate is known, then these equations can be revised to permit the determination of the parameters of the equation. If the viscometer is designed in such a way that the relative gap $|(R_2 - R_1)/R_2|$ is quite small, then the shear rate becomes nearly constant across the gap, and the shear rate can be calculated using the approximate expression shown in Equation 9.

For the Laray viscometer used in this study the gap was 3×10^{-5} m, and the variation in shear rate across the gap was estimated to be less than 1 per cent. Under these circumstances, the viscosity can be calculated using Equation 10.

Or, in terms of the mass, M:

However, if the fluid is thixotropic, i.e. if its viscosity depends not only on the rate of shear but also on the length of time it has been sheared, then there is no straightforward method to obtain well-defined rheological properties using a falling rod viscometer. This is because the total viscous force resisting the fall of the rod is the resultant of shear stresses contributed by fluid elements that have been sheared for various lengths of time. If the approach of the viscosity to its equilibrium value is rapid, as it often is at high shear rates, and if the total time of shearing for a fluid element (proportional to L/V) is relatively long, then the viscosity calculated using Equation 10 may still be a reasonable approximation of the true viscosity at the shear rate given by Equation 9.

To carry out a test using the falling rod viscometer a small quantity of ink (3-5 cm³) is applied to the lower end of a metal rod that serves as the inner cylinder. The rod is then dropped through the stationary outer cylinder, coating the shearing surfaces with a thin film of ink. Since the gap is very small the ink film acts as a rod centering mechanism, so that the rod and cylinder can be assumed to be concentric. The rod is subsequently pulled back up through the outer cylinder, and excess ink is scraped off the rod into the funnel-shaped entrance of the outer cylinder. A variety of weights can be added to the top of the rod, increasing the shear stress imposed on the ink film. The rod is then released, and the time (t) required for it to fall a fixed distanced (H) is measured by means of two photoelectric cells connected to an automatic timer. The velocity is then determined as follows:

$$V = H/t$$

The Laray viscometer located in the Canada Printing Ink manufacturing control centre in Montreal was used for this study. The ambient temperature during the ink viscosity measurements was $27.3 \pm 0.2^{\circ}$ C. The outer cylinder was in contact with a cylindrical metal jacket through which flowed a steady stream of liquid from a temperature controlled bath (32.3°C). The temperature of the Laray outer cylinder was monitored by means of a thermocouple placed in an oil-filled well drilled in the side of the cylinder. This temperature, which was displayed on a digital readout, ranged between 31.0°C and 32.0°C.

The passage of the rod through the cylinder reduced the gap temperature during the initial and middle span of the fall-time of each ink. This is because of the cooler rod and ink pool at entrance to the gap, since they are affected by the ambient temperature, which was lower than the temperature of the water bath. Precautions were taken prior to each test run to ensure that the annulus temperature had reached its equilibrium (\simeq 31.4°C) value.

The rod mass was 130 g, and 25, 50, 100, 150, 200, 300 and 500 g metal weights were added to provide data for a wide range of shear stresses.

Reproducibility was found to be poor at small loads, but this viscometer is not intended for use at low shear stresses. Values of the shear rate and viscosity, calculated using equations 9 and 10, are listed in Table 3 for the largest weight used to study each ink. Also listed are the values of the paramater, $\eta_{\rm cs}$ determined from experiments in the Mechanical Spectrometer.

It should be noted that the temperature used for the latter experiments was 30° C, while the nominal temperature for the Laray experiments was 31.5° C. This is a probable explanation for most of the difference between the two values, as temperature is known to have a strong effect on viscosity. Since the variation of viscosity with temperature varies from one fluid to another, we would not expect to observe the same ratio of the two viscosities for all the inks.

To throw further light on this question, the Laray viscometer was also used to study a series of solutions of resin in oil, which should not be thixotropic. The results are shown at the bottom of Table 3. A definite pattern can be seen in which the ratio of the two viscosities is correlated with the carbon black content, decreasing from about 0.5 to 0 per cent carbon black to about 0.27 for 20 per cent carbon black. This seems to reflect a decreased variation of viscosity with temperature as carbon black is added.

Evaluation of the Inkometer

The Inkometer was originally developed by Reed¹² to simulate, on a laboratory scale, the processes occurring as ink flows through a printing roller nip. The essential features of this type of tackmeter are illustrated in Figure 4. Cylinder B is motor driven at a constant speed, while cylinder C rotates and reciprocates along its axis to generate a homogeneous ink film. Stress is transmitted from cylinder B to cylinder A by the ink and results in a net force on cylinder A in the direction "R". The force in the "L" direction required to prevent the displacement of cylinder A is measured and is proportional to the Inkometer Number (IN).

 Table 3

 Comparison of ink viscosities determined by two methods

Ink no.	η∞(Pas) (Eqn. 4)	η (Pas) (Eqn. 11)	γ̈́(s ^{−1}) (Eqn. 9)	<u>η(Laray)</u> η _∞	%C
1	1.826	0.835	1583	0.457	8
5	1.857	2.485	1511	1.338	8
9	3.026	1.160	1749	0.383	14
13	6.673	1.710	1187	0.256	20
17	6.788	1.771	1146	0.261	20
6	7.483	2.993	678	0.400	8
2	7.963	3.054	665	0.384	8
4	8.562	3.481	583	0.407	8
10	9.460	3.579	1749	0.378	14
8	12.287	3.937	755	0.320	14
12	13.874	4.474	665	0.322	14
14	23.732	7.329	277	0.309	20
16	27.070	7.390	275	0.273	20
18	27.257	7.451	405	0.273	20
3	41.875	13.314	152	0.318	8
7	58.351	19.422	104	0.333	8
11	84.253	39.193	76	0.465	14
% Varnish		Varnish-oil S	Solutions		
0	1.111	0.621	1749	0.5	
9.9	3.511	1.832	1108	0.522	
12.5	5.275	2.626	773	0.498	
15.0	7.744	3.848	528	0.497	
17.5	11.959	5.741	354	0.480	
20.1	19.915	9.222	220	0.463	



Figure 4. Principal features of the Inkometer

The work of Mewis and Dobbels¹³ has shown that tackmeters of this type do not, in fact, simulate the printing process. The force measured is strongly dependent on the loss tangent of the viscoelastic rubber covering cylinder A, and there is no way to scale-up tackmeter results so that they are quantitatively relevant to press behaviour. Other types of tackmeter have been developed more recently¹⁴ which make a less ambiguous measurement of tack. Nevertheless, these devices continue to be used to compare inks, and it is of interest to know something about the reproducibility of the test

results and their possible correlation with rheological properties.

The Inkometer employed in this study was manufactured by Thwing-Albert (Model No. B-45; Serial No. 29242). The central, metal-covered cylinder could be driven at three rotational speeds, and the results reported here were obtained using the medium speed. A small amount of ink (2-3 cm³) was applied to the Inkometer cylinders while the motor was turned off. The applied ink was then spread over the three cylinders by manually rotating the central cylinder. After three full rotations, the motor was started and the Inkometer Number was determined as a function of time. Replicate runs indicated that the results were quite reproducible.

Figures 5 to 7 are curves of IN versus time for the inks used in this study, while Figure 8 shows similar results for several solutions of varnish in oil. The Inkometer Number varies markedly with time in the early stages of the measurement, usually reaching a steady state value after several minutes.

The transient nature of the Inkometer reading requires that the measurement of the IN always be made at the same time after starting the motor. The initial peak is believed to depend on the mass of ink initially present and on the degree of uniformity in the ink film. The sharp initial decrease in IN is probably due to the loss of fluid as a result of misting. Misting was especially pronounced in the case of the varnish solutions. As can be seen in Figure 8, the transient curves for these materials are more complex in shape. It is possible that the second maximum is a viscoelastic effect. The presence of carbon black appears to suppress this aspect of the response.

No simple correlation could be found between ink composition and IN. In Table 4 the inks are listed in order of increasing IN, and the value of η_{∞} is also shown. The ranking according to η_{\circ} is similar but not identical. Thus, while IN does not have a simple correlation with η_{∞} , high shear rate viscosity clearly plays an important role in ink flow in an Inkometer.

Conclusions

The rheological measurements performed on a Rheometrics

Table 4						
Ranking	of	Inks	according	10	Inkometer	Number

Ink Number	Equilibrium Inkometer Number	η _α (Pas) (Eqn. 4)
1	2.4	1.826
5	2.5	1.857
9	3.0	3.026
13	3.5	6.673
17	4.0	6.788
2	5.0	7.963
8	6.1	12.287
10	6.3	9.810
6	8.0	7.483
14	9.0	23.732
4	9.2	8.562
12	10.0	13.874
16	10.5	27.070
18	11.0	27.757
3	21.7	41.875
7	25.6	58.351
11	28.7	84.253
15	34.8	
19	40.5	



Figure 5. Inkometer number versus time for inks 6, 8 and 14. All three had a resin content of 9.9 wt per cent



Figure 6. Inkometer number versus time for inks 4, 9, 10, 11 and 16

Mechanical Spectrometer revealed that the inks display shearthinning behaviour, thixotropy, yield stress, and a shear stress response that is dependent on the nature and duration of previous shear. The addition of carbon black increases the



Figure 7. Inkometer number versus time for inks: 3, 7, 11, 15 and 19. All had a resin content of 20.1 wt per cent



Figure 8. Inkometer number versus time for resin – Oil Solutions (varnishes) with resin concentrations up to 20.1 wt per cent

equilibrium viscosity and the yield stress of an ink, while the addition of pitch reduces the low shear viscosity.

The Laray viscometer was found to yield a reasonably precise value of the steady shear equilibrium viscosity of the inks at high shear stresses. The Inkometer, while neither measuring any well-defined physical property nor simulating in any quantitative sense the printing process, does provide an interesting characterization of the inks. The fact that the ranking according to equilibrium Inkometer Number varies from the ranking according to high shear viscosity emphasizes that the flow in the nip cannot be analyzed solely through the use of steady shear results. Thus, although the Laray gives a good steady shear rheological characterization of the inks, this is not directly relevant to nip flow.

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Dispersion of cuprous oxide in antifouling paints. Coefficients defining particle shape and size

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Introduction

The main objective of pigment dispersion in the paint manufacture process is separating clustered particles and keeping them permanently isolated from each other.

As a general rule, particles are associated in the form of clusters due to their high surface force (high free energy per mass unit). These aggregates may appear after the evaporation of the washing liquids due to the incipient sintering, when high temperature methods are used in obtaining the pigment, or as a result of compacting forces applied during the storage of the packed pigment. However, the size of the primary or individual particles is generally sufficiently small and thus appropriate for its utilization in industrial processes.

During pigment dispersion in the vehicle there is an initial air displacement due to a flow of the vehicle in the interstices of the pigment mass. This wetting process depends on the viscosity of the vehicle and on the compaction degree of the agglomerates. Even under favourable conditions (low vehicle viscosity and high solid porosity) the dispersion process requires mechanical energy so as to wet the particles and, additionally, to produce stable separation. The latter is attained when each one of the particles remains surrounded with a sufficient amount of the vehicle, thus avoiding contact with the other particles.

If dispersion stability is not appropriate, particles join again and form floccules. The floccules are associations that may include from a few to hundreds of primary particles 1.2.

The shape and the size of the particles show a significant influence upon the various paint characteristics, such as: hiding power, rheological behaviour, film aspect and gloss retention, durability and resistance to chalking, checking and cracking.

The objective of this paper is to determine coefficients that may serve to define the shape and the size of discrete or individual particles and of associations of the latter.

Method

In order to perform these experiments, four commercial

samples of cuprous oxide were selected. This is a pigment that is commonly used as toxicant in antifouling paints. Figure 1 shows characteristics of the particles in this pigment as viewed through an electronic microscope (enlarged 1,000 and 5,000 X).

The selection of cuprous oxide for these experiments was made based upon the fact that its particle size distribution plays an important role in the biocide power of antifouling paints.

Specific area of the discrete particle

Both the shape and the size of the particles and dispersion efficiency refer to the external area of the solid body. Since calculating the number of particles included in a mixture is unpractical, the basis for evaluating the surface is by considering the mass unit. In this way the idea of specific area is established. This value, multiplied by the sample mass, defines the interfacial area. The specific area is an important property of solid bodies and varies significantly with the characteristics of the interfacial area and the size of the particles.

The specific area can only be calculated if the geometrical shape of the particles is known. In the case of spheres, the superficial area is IId2, where d is the diameter, the mass being $\rho IId^{3}/6$, where ρ is the density. Consequently the specific area of a spheric particle becomes 6/pd.

However the geometrical shape is usually different and, therefore, the specific area cannot be calculated by means of the above expression. For this reason, the specific area of the discrete or individual particles has been determined by means of an Accusorb Micromeritics Absorption Unit, based on the BET theory³. This was performed after degassing the samples by high vacuum during two hours and at 150°C.

Specific area of particle associations (aggregates)

In the case of associated particles, the superficial area was determined on the basis of the specific dissolution rate of cuprous oxide in an 0.48 M sodium chloride solution, with pH 8.2 and at 20°C temperature. Starting from experimental dissolution time and dissolved mass of cuprous oxide, the

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Figure 1. Electron microscope view of cuprous oxide samples. The top picture shows magnification of \times 1,000, the bottom one shows a magnification of \times 5,000

evaluation was performed with wholly deflocculated particles (this was verified microscopically).

The mean specific area of associated particles was assessed by relating the previously determined area with the dispersed cuprous oxide mass.

Five dispersion times were selected so as to obtain different mean particle size. The maximum cuprous oxide concentration in the solution⁴ was 0.5 ppm. This was established colorimetrically⁵.

Mean diameter of associated particles (aggregates)

The diameter of discrete particles (d), and that of the aggregates (D), was assessed microscopically. The correspond-

ing mean diameters \overline{d} and \overline{D} were calculated using the following formula:

Σ f (diameter)² / Σ f

where f is the frequency at which each particle or particles association is present in the dispersion. The word diameter refers to the values of d or \bar{D} .

Shape and size correction factors

The following experimental relations are defined:

- 1. Shape factor of individual or discrete particles (f_1) . It relates the real specific area of the discrete particles obtained through BET with that corresponding to the discrete particles calculated as spherical, starting from diameter d, by means of the expression $6/\rho d$.
- 2. Shape factor of the aggregates (f_2). It relates the surface area of particles associations with that calculated as spherical, starting from diameter \overline{D} , by means of the expression $6/\rho d$.
- 3. Size factor of the aggregates (f_3) . It relates the real specific area of the discrete particles obtained through BET with that of the associated particles.
- 4. Size and shape factor of the aggregates (f_4). It relates the real specific area of the discrete particles obtained through BET, with that of the particles associations calculated as spherical, starting from diameter \overline{D} , by means of the expression $6/\rho\overline{D}$.

Table 1						
Composition	of	cuprous	oxide	samples,	g/100 g	

Sample	Cuprous copper*	Cupric copper†	Metallic copper
1	99.81	0.04	0.03
2	99.22	0.51	0.11
3	98.17	1.33	0.23
4	97.71	1.57	0.31

*Shown as cuprous oxide (Cu₂O) †Shown as cupric oxide (CuO)

Table 2 Characteristics of the tested samples

Sample	Diameter d µm	Specific area cm ² g ⁻¹	Dissolution rate µg cm ⁻² day ⁻¹
1	0.4	30 800	255
2	0.7	18 200	248
3	1.1	12 070	246
4	1.3	10 699	239

Results and conclusions

The samples of cuprous oxide selected for the experiment, after eliminating the stabilizer by washing, show the composition indicated in Table 1.

Table 2 shows the diameters and specific areas of the discrete particles for each one of the samples, as well as the specific dissolution rate in the aqueous solution mentioned above.

These experimental results allowed the calculation of factor

 f_1 (shape of the discrete particles) for each one of the pigment samples selected. Figure 2 shows the values of this factor as a function of the mean diameter of the particles. Direct proportionality may be observed for both values of the specific area. Since the value $f_1 = 1$ indicates spherical particles, this factor shows in how much discrete particles differ from sphericity. Thus, a mathematical quantization has been obtained for the shape of the individual particles.

Table 3 shows the specific area of the associated particles, whose determination involved the evaluation of the specific dissolution rate by means of the above mentioned methodology as a function of mean diameter \overline{D} .



Figure 2. Separation from sphericity of discrete particles as a function of their mean diameter



Figure 3. Separation from sphericity of particles associations as a function of their mean diameters

Factor f_2 (shape of the aggregates) is shown to be, as with f_1 , directly proportional to the mean diameter of the associated partiles \overline{D} (Figure 3).

Figure 3 also shows that, for an equal mean aggregate diameter (\overline{D}) , discrete particles with a greater mean diameter (\overline{d}) lead to particles associations that farther differ from sphericity (larger shape factor f_2). This means that these associations have a larger real specific area.

Factor f_2 proved to be relevant, since for a given cuprous oxide dispersion, it allows the calculation of the real specific area of the aggregates.

With regard to factor f_3 (size of the aggregates), it must be noted that it is related to dispersion efficiency (Figure 4). For a given size of discrete particles, a larger factor f_3 indicates a larger mean diameter (a higher number of discrete particles and a larger specific area of associated particles) and, therefore, lower dispersion efficiency.

Table 3Specific area of associated particles (aggregates)

Discrete particle	Associated particles				
d, μm	D̄, μm	A, $cm^2 g$			
0.4	2.9	5 050			
0.4	5.4	2 750			
0.4	7.6	1 967			
0.4	8.1	1 846			
0.4	11.3	1 341			
0.7	3.6	4 103			
0.7	5.2	2 860			
0.7	8.5	1 774			
0.7	10.6	1 4 5 1			
0.7	11.2	1 392			
1.1	6.4	2 328			
1.1	7.6	1 974			
1.1	9.6	1 584			
1.1	10.9	1 4 3 2			
1.1	12.2	1 312			
1.3	7.3	2 058			
1.3	9.1	1 673			
1.3	11.7	1 388			
1.3	13.0	1 312			
1.3	13.5	1 293			



Figure 4. Relative index of the number of discrete particles involved in the aggregates, as a function of their mean diameters



Figure 5. Relation between the specific area of discrete particles and that of particles associations, as a function of the mean diameters

All this led to the conclusion that factor f_3 is a relative index of the number of particles involved in the association.

The definition of the factor f_4 (shape and size of the aggregates), and the experimental values obtained for factors f_1 ,

and f_3 , lead one to conclude that f_4 is equal to the product of f_2 by f_3 , and since f_3 is higher than f_2 , the behaviour of f_4 follows that of f₁.

The significance of factor f_4 is given by the fact that the specific area of the discrete particles obtained by dispersion of cuprous oxide may be calculated by multiplying the specific area of the associated particles, as from \overline{D} , by factor f_4 taken from Figure 5 for the corresponding d value.

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Styrenated alkyd resins based on maleopimaric acid

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Abstract

Unstyrenated alkyd resins were prepared from maleopimaric acid and phthalic anhydride separately using monomeric dehydrated castor oil. These alkyds were styrenated using the post-styrenation process by addition of tung oil and using benzoyl peroxide as an initiator. The styrenated alkyd films showed an improvement in film properties; such as drying time, scratch hardness, rocker hardness, resistance towards water, and acid and alkali; over the unstyrenated alkyd films. Both the styrenated alkyd films, based on maleopimaric acid and phthalic anhydride, behaved in exactly the same way for all the film properties except hardness. Baked films showed an improvement in all the film properties over air-dried films.

Introduction

Styrenated alkyds may be considered to be resin modified alkyds; the resin being polystyrene. Polystyrene is tougher and more durable than the natural resin-modifiers generally used, and the styrenated alkyds show similar advantages of better toughness and durability. Polystyrene has good resistance to water and alkalies and this quality is imparted to the styrenated alkyd. The styrenated alkyds have established a definite position in the field of fast air-drying and baking finishes.

There is hardly any information available on copolymerisation of non-phthalic alkyds with styrene. However, some information is available on copolymerisation of oils and conventional phthalic alkyds with styrene. Non-phthalic alkyds are essentially oxidising resins in which phthalic anhydride has been replaced by fatty acid-maleic adduct, rosin-maleic adduct, and maleopimaric acid, trimellitic acid, succinic acid, etc. The copolymerisation of oils with styrene has been extensively studied by several workers1.8. Bhow and Payne9 studied styrenated DCO-phthalic alkyd resin prepared by first styrenating the DCO fatty acids and then allowing them to react with phthalic anhydride and glycerol. Evaluation of these styrenated alkyds showed that they had superior drying times and chemical resistance to the conventional phthalic alkyds. According to Heavers¹⁰ the styrenation of phthalic alkyds

results in improved hardness and resistance to acids and alkalies. Bevan et al¹¹ correlated the film properties of vinyl hydrocarbon modified phthalic alkyd resins based on linseedtung oil and tobacco oil-DCO and reported that the later crosslinked more readily than the former in spite of lower total unsaturation and lower degree of conjugation. Gupta et al12 prepared styrenated phthalic alkyds based on babul oil (Acacia arabica) by pre-styrenation and post-styrenation processes and their film properties were compared with those of unstyrenated tobacco seed oil alkyds. The alkyds prepared by the post-styrenation process gave better film properties than the alkyds prepared by the pre-styrenation process. Shukla et al¹³, prepared styrenated tobacco oil phthalic alkyd by prestyrenation and post-styrenation processes and studied the film properties of their air-dried as well as baked films along with those of unstyrenated tobacco oil alkyds.

In the present work, non-phthalic alkyd resin has been prepared from maleopimaric acid. The styrenation of the nonphthalic alkyd and the conventional phthalic alkyd has been achieved by a post styrenation process. The properties and performance characteristics of these alkyds have been compared with each other.

Experimental

Materials

Dehydrated castor oil (DCO): Commercial acid value 5.1, iodine value 136.0, hydroxyl value 18.0, viscosity (25°C) 2.0 poises, and colour 16.8Y + 2.1R.

Tung oil: Acid value 3.6, viscosity (at 25°C) 4.0 poises, iodine value 161.0, and colour 20.4Y + 7.6R.

Glvcerol: Sarabhai Merck, LR grade.

Ethylene glycol: Sarabhai Merck, LR grade.

Phthalic anhydride: LR grade.

Maleopimaric acid (Prepared in laboratory): Acid value 420.0, melting point 228.5°C, optical rotation | α β5°C - 32.1.

Table 1 Styrenation of alkyds in xylene at 140°C for 20 hours with benzoyl peroxide initiator

C No	Initiator	Clarity					
5. INO.	(% by wt of alkyd)	Styrenated maleopimaric non-phthalic alkyd	Styrenated phthalic alkyd				
1.	1.0	Hazy	Hazy				
2.	1.5	Hazy	Hazy				
3.	2.0	Hazy	Hazy				
4.	2.5	Slightly hazy	Hazy				
5.	3.0	Clear	Slightly hazy				
6.	3.5	-	Clear				

Styrene monomer: LR grade, refractive index (at 30°C) 2.5423, specific gravity 0.9108, boiling range 140-145°C. Benzoyl peroxide: LR grade.

Xylene: LR grade, sulphur free, boiling range 137-142°C.

Red oxide of Iron: Commercial, synthetic, Fe_2O_3 content 93.6 per cent.

Zinc chrome: Commercial Cr_2O_3 content 45.6 per cent.

Cobalt naphthenate: Metal content 4.5 per cent.

Preparation of alkyds from maleopimaric acid

DCO and glycerol were reacted in a three-necked flask fitted with stirrer, condenser and thermometer. Inert gas (N₂) was passed into the reaction mixture through a glass tube. The mixture was heated to 200°C and 0.1 per cent catalyst (lime and litharge in a ratio of 1:1) of the weight of the oil was added. The temperature was raised to 240°C and maintained there for one hour after which the temperature was lowered to 200°C. At first, ethylene glycol and thereafter maleopimaric acid were added slowly to the reaction mixture. The temperature was raised to 250°C gradually and maintained until the desired acid value and viscosity were obtained. The formulation of the alkyd based on maleopimaric acid was as follows:

Ingredients	Parts by weigh			
DCO	600			
Maleopimaric acid	240			
Glycerol	50			
Ethylene glycol	25			

Preparation of alkyds from phthalic anhydride

DCO and glycerol were heated to 200°C in a three-necked flask fitted with a stirrer, a gas inlet tube and a thermometer. Catalyst (lime and litharge in the ratio of 1:1), 0.1 per cent of the oil weight, was added to the reaction mixture and the temperature was raised to 240°C slowly. The temperature was kept constant until monoglyceride tolerance in methanol (1:3) was obtained, after which DCO fatty acid and phthalic anhydride were added slowly to the reaction mixture at 180°C. The temperature was further raised to 240°C and maintained there until the desired acid value and viscosity were reached. The formulation of the phthalic alkyd was as follows:

Ingredients	Parts by weight
DCO	340
DCO fatty acids	232
Phthalic anhydride	200
Glycerol	108

Preparation of styrenated alkyd from maleopimaric acid

In a typical experiment the alkyd, tung oil and xylene were placed in a three-necked flask with thermometer, condenser and stopper. The requisite amount of initiator was added in the reaction mixture and the temperature raised to 140° C (refluxing temperature). At this stage, half the amount of styrene monomer was added to the flask. The remaining quantity of styrene was added after two hours refluxing and the refluxing continued for 20 hours. After this period xylene was removed by vacuum distillation until a product having 50 per cent solids was obtained. Different concentrations of initiator were tried. The results are shown in Table 1. The final product was prepared according to the following formulation:

Parts by weight		
300		
30		
300		
900		
9		

Preparation of styrenated alkyds from phthalic anhydride

The procedure adopted for preparing styrenated phthalic anhydride based alkyds was the same as that described above for preparing styrenated alkyd from maleopimaric acid. In this process too, different percentages of initiator were tried. Except for the amount of initiator used in this case which was 3.5 per cent on the weight of alkyd taken for styrenation, the proportions of the other ingredients were the same. The results are shown in Table 1.

Preparation of paints from styrenated alkyds

For this purpose, red oxide zinc chromate primers were prepared from both the styrenated alkyds separately as follows by the usual procedure. The composition of the primer paint was as follows:

Ingredients	Parts by weight
Red oxide of iron	42.00
Zinc chrome	8.00
Styrenated alkyd (50% solution in xylene)	50.00
Cobalt naphthenate (4.5% Co)	0.17

Characterisation and evaluation of film performance of styrenated alkyds

The physico-chemical characteristics of both the styrenated alkyds such as clarity, acid value, viscosity, and colour, were determined and the results are given in Table 2.

The film properties of both air dried and baked films of styrenated alkyds were determined and the results are given in Table 3. The film characteristics of the primers are given in Table 4.

Results and discussion

The different experiments of styrenation of non-phthalic alkyd based on maleopimaric acid were carried out by varying the amount of initiator and solvent, separately. The process adopted for styrenation of this alkyd was post-styrenation. In all the experiments, hazy products were obtained. This may be due to the fact that the maleopimaric acid molecule is bulky in nature which causes some stearic-hinderances on the double

	Table 2			
Characteristics	of unstyrenated	and	stvrenated	alkyds

SI. No.	Product	Acid value	Viscosity of 50% solution in xylene at 25°C (Poise)	Colour of 50% solution in xylene (Lovibond unit)
۱.	Unstyrenated alkyds	5		
	 Maleopimaric non-phthalic alkyd 	16.1	0.5	22.0Y + 5.5R
	(ii) Conventional phthalic alkyd	16.6	0.5	25.4Y + 6.3R
2.	Styrenated alkyds			
	 Maleopimaric non-phthalic alkyd 	19.3	1.0	25.8Y + 6.2R
	(ii) Conventional phthalic alkyd	19.4	0.5	27.2Y + 7.3R

bonds of the alkyd resin molecule which would result in a higher rate of homopolymerisation of styrene than copolymerisation with alkyd resin – thus causing haziness in the product. To avoid this problem, further experiments of styrenation of this alkyd were conducted by blending 10 parts of tung oil with 100 parts of alkyd resin. For the purpose of comparing the film properties, the conventional styrenated phthalic alkyd was also prepared by blending tung oil with phthalic alkyd with same level as in the case of styrenated nonphthalic alkyd based on maleopimaric acid.

Characteristics of styrenated alkyds

Table 2 shows the characteristics of unstyrenated and styrenated alkyds prepared from maleopimaric alkyd and conventional phthlatic alkyd. On the perusal of table, it is observed that acid value increased from 16.1 to 19.3 during styrenation in the maleopimaric alkyd and from 16.6 to 19.4 in the phthalic alkyd. There was greater increase in the viscosity of maleopimaric acid based alkyd as compared to phthalic alkyd after styrenation. There was also a slight increase in colour of the alkyds during styrenation in both cases.

Film properties of styrenated alkyds

The film properties of styrenated and unstyrenated alkyds and red oxide-zinc chromate primers based on styrenated alkyds are shown in tables 3 and 4 respectively.

Drying Time

All the alkyd solutions were applied to mild steel panels by brush and dried in air. Drying time was checked by the touch method for different stages of the coatings, i.e. surface dry, hard dry, and freedom from tack. The improvement in the drying time after styrenation in the air dried films is very significant as is apparent from the results. The surface drying time after styrenation was reduced by a quarter, i.e. from 2 hours to 0.5 hours, the hard drying time from 8 hours to 4 hours and tack-free period from 36 hours to 18 hours. The drying properties of both the alkyds were otherwise the same.

Scratch and rocker hardness

Scratch hardness of the dried films (48 hours, air dried or baked) were checked on tin plate using a mechanically operated 'Sheen' scratch hardness tester. The rocker hardness was tested on glass panels and rocker value determined with respect to glass. Scratch hardness as well as rocker hardness of the baked films were slightly higher values than for the corresponding air-dried films. Significant improvement in the hardness of films was observed due to styrenation. Films of maleopimaric acid based alkyd showed comparatively better hardness than conventional phthalic anhydride based films. The primer films of styrenated alkyd based on maleopimaric acid also showed a better scratch hardness value than styrenated alkyd based on phthalic anhydride.

Flexibility

Flexibility testing of the films were done after 48 hours air drying or baking at 120°C for 30 minutes on a quarter inch mandrel. This test was carried by coating the samples on tin plate. All the alkyd films (styrenated as well as unstyrenated) showed no detachment of the film from the substrate or visible cracks, indicating that all the samples had good flexibility.

Impact resistance

This was carried out on coated tin plates after 48 hours air drying or baking at 120°C for 30 minutes. A weight of 2 lbs was allowed to fall a height of 24 inches and any damage, such as cracking or detachment of the film, was noted with the help of a magnifying glass. All the films passed the impact resistances test.

Water resistance

This was determined by immersing the coated glass panels in distilled water for desired periods. They were then taken out and dried in air. The defects, if any, such as blushing, swelling, cracking, wrinkling and loss of gloss of the air-dried and baked films of styrenated alkyds were studied. No such defects on the films were observed after immersion in water for 48 hours in case of styrenated alkyds. However, the air-dried films of unstyrenated alkyds showed slight loss of gloss after 48 hours. Styrenated alkyds of the air-drying type showed loss of gloss after 96 hours. Styrenated anafter 96 hours of immersion while the baked films remained unaffected.

Acid resistance

The coated and dried glass panels were immersed in 2 per cent sulphuric acid for a specified period. The panels were then taken out gently, washed with distilled water, dried, and films examined for any defects as pointed out above in the water resistance test. The acid reistance of all the alkyd films was generally good. No effect of sulphuric acid immersion was observed in any of the films after 48 hours. However, after 96 hours immersion, all unstyrenated alkyd films (both air dried and baked) showed slight loss in gloss.

Alkali resistance

This was determined by immersing glass panels in 2 per cent sodium carbonate solution. Thereafter the panels were washed with distilled water, dried and observed for any damage as above in water resistance. The styrenated alkyds showed good resistance to alkali.

These alkyd films remained completely unaffected by 2 per cent sodium carbonate solution during immersion for 8 hours whereas the corresponding unstyrenated alkyd films were removed during this period of immersion in alkali. However, during the first 4 hours of immersion in alkali all the films remained unaffected.

Solvent resistance

The coated glass panels were immersed in mineral terpentine oil. After the specified period the panels were taken out, dried in air and examined for any damage to the films as above in water resistance. The resistance to mineral turpentine oil was good for all the styrenated alkyd films, and no effect on these

				Table 3					
Comparison	of film	properties	of air-driea	films o	of the	styrenated	and	unstyrenated	alkyds

Product	Di	ying ti	me	Hard	dness	Flexibility	Impact	Wa	ater	Ac	cid ist-	All	cali ist-	Sol	vent
	SD	HD	TF	Scra- tch	Rock- er	adhesion	2 lbs from	ance		ance H ₂ S	(2%) 50 ₄	ance Na ₂	(2% CO ₃	an (M.1	ісе Г.О.)
				(gm)		mandrel	24" height	48 hrs	96 hrs	48 hrs	96 hrs	4 hrs	8 hrs	24 hrs	48 hrs
Air dried 1. Unstyrenated maleopimaric non-phthalic alkyd	2	8	36	1400	14	Р	Р	4	3	5	4	5	1	5	4
 Unstyrenated conventional phthalic alkyd 	2	8	36	900	10	Р	Р	4	3	5	4	5	0	5	4
3. Styrenated maleopimaric non-phthalic alk vd	0.5	4	18	1850	28	Р	Р	5	4	5	5	5	5	5	5
 Styrenated conventional phthalic alkyd 	0.5	4	18	1550	16	Р	Р	5	4	5	5	5	5	5	5
Baked I. Unstyrenated maleopimaric non-phthalic alkyd	-	-	-	1400	20	Р	Р	5	4	5	4	5	1	5	4
2. Unstyrenated conventional phthalic alkyd	-	-	-	1050	14	Р	Р	5	4	5	4	5	0	5	4
 Styrenated maleopimaric non-phthalic alkyd 	-	-	-	2000	32	Р	Р	5	5	5	5	5	5	5	5
 Styrenated conventional phthalic alkyd 	-	-	-	1800	20	Р	Р	5	5	5	5	5	5	5	5

5 = Film practically unaffected; 4 =Slight loss in gloss; 3 =Slight blushing and loss of gloss; P =Pass; 2 =Heavy blushing and complete loss of gloss; 1 =Partial film lift off; 0 =Complete film lift off.

Sr. No.	Product	Drying time in hours (hard dry)	Finish	Scratch hardness (gm)	Flexibility and adhesion	Corrosion resistance (7 days)	Salt spray resistance (4 days)
1.	Styrenated maleopimaric non-phthalic alkyd based primer	3.0	Matt	1800	Р	Р	Р
2.	Styrenated conventional phthalic alkyd based primer	3.0	Matt	1600	Р	Р	Р

Table 4 Film properties of red oxide-zinc chromate primer

films was observed afer 48 hours immersion. The unstyrenated alkyds however, showed slight loss in gloss after 48 hours immersion.

Corrosion resistance

The mild steel panels coated with the paints were air dried for 24 hours followed by baking at 60° C for one hour. The panels were then suspended in a corrosion cabinet. The latter was maintained at 100 per cent relative humidity and temperature cycle of 42° to 48° C for seven days. The panels were examined for any signs of deterioration in the film due to corrosion of the metal surface. Both primer films passed this test.

Salt spray resistance

The paint coated mild steel panels were dried as above and suspended in a salt spray chamber for 4 days. They were then taken out and examined for any signs of deterioration and corrosion exactly as described in corrosion resistance test. Both primer films passed this test also.

Conclusions

Significant improvement in the drying properties of the alkyds takes place upon styrenation. The hardness and other film properties of the alkyds, such as water, acid, alkali and corrosion resistance are also improved. This is due to the fact that polystyrene has excellent resistance to water, acid and alkali which is partially imparted to the alkyd resin after styrenation. Further improvement in the film properties of the styrenated alkyds can be achieved by drying the films by baking which results in further polymerisation. This significantly improves the film characteristics and general performance of the alkyd resins.

The above results indicate that the styrenated alkyds based on maleopimaric acid may be used in fast air drying coatings, anticorrosive coatings, industrial finishes, etc., in place of styrenated phthalic alkyds.

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next month' inve

The Honorary Editor has accepted the following papers for publication in the April issue.

Filtration of surface coatings by C. G. Roffev

Measurement of film thickness by colour comparison using primers with low opacity by M. Camina and W. Bainbridge Development of wood varnishes from palm fruit fibre hydroxylate (eheis guineensis) and red onion skin (allium cepa) tannin extract by T. O. Odozi, O. Akaranta and I. U. Ogban

occa meeting

Ontario Section

Can you measure up to the future

The second technical meeting of the Ontario Section's 1984-85 session was held on 17 October 1984 in the Cambridge Hotel, Toronto. Continuing a recently established tradition, this meeting was held primarily for the benefit of our students.

Forty-seven members and guests turned out to listen to Mr David O'Donnell, president and chief executive officer of Sinclair, Valentine and Frye, Canada.

Mr O'Donnell opened by complimenting the Ontario Section for its fine Printing Ink Technology Course and the benefits it has had, and will continue to have, for the industry. He commented that the ink industry was currently undergoing great change and that technology advancements made in the last five years were greater than anything achieved in the previous fifty years.

Encouragement was given to the students in their endeavours as more and more young people were aspiring to positions of responsibility within the ink industry. Mr O'Donnell then gave some examples of the areas of increased sophistication in his company and stressed that their increased commitment to R & D required highly trained and dedicated personnel to achieve success in a very competitive world.

Mr Purnell then presented Mr O'Donnell with a certificate acknowledging his presentation and proposed a vote of thanks. Those present responded in the normal manner.

Dispersion equipment

Forty-eight members and guests were present at the technical meeting held in the Cambridge Motor Hotel on 18 November 1984. The speaker was Mr Gerry Brussard, President of Chemitrade Inc. who gave a presentation on "Dispersion Equipment"

In spite of the fact that his slides were held up by Customs, Mr Brussard was able to overcome this handicap and give an interesting and informative lecture. He described new developments in premixing technology by "Draiswerke", where significant improvements in efficiency were claimed. He went on to describe "direct dispersion equipment" in which the bead or shot mill was connected directly to a mixing and feeding assembly. This enabled dry ingredients, such as pigment, and liquid ingredients such as vehicle and solvent, to be continuously fed into the system in the correct proportions for mixing and dispersion. Savings in increased efficiency and reduced manpower were claimed.

A lively question and answer period ensued, followed by a vote of thanks proposed by the Chairman.

P. Marr

Natal Section

Concepts in emulsion polymerisation

On Wednesday 7 November 1984, Mr Terry Say, technical director of Bevaloid (SA) (Pty) Ltd, and current Chairman of the Natal Section, gave a lecture entitled "Concepts in emulsion polymerisation".

Mr Say first outlined the basic concepts of addition and condensation polymerisation and then detailed the advantages and disadvantages related to each technique. Components of an emulsion polymerisation system were listed with the resultant effect of monomer composition on paint properties. The importance of surfactant balance was stressed, with greater amounts needed when the surface to volume ratio increased. Paint properties affected by emulsion characteristics were listed in detail and the effects of catalysts, molecular weight modifiers, pH buffers, biocides and coalescing solvents were explained. Finally, the kinetics of emulsion polymerisation in relation to the Smith-Swart and Medvedev-Sheinker theories were discussed.

occa meeting

The lecture was well documented with slides and a lively question time ensued from the attentive audience. The vote of thanks was proposed by Mr N. Grey who also thanked Messrs Bevaloid for sponsoring the evening's refreshments.

R. Philbrick

Manchester Section

Recent developments in synthetic resins

On Monday 12 November 1984, seventy members and guests of the Manchester Section attended a lecture by Mr A. G. North of Cray Valley Products entitled "Recent developments in synthetic resins". The lecture at the Georgian House, Blackrod, was followed by an excellent buffet sponsored by Cray Valley Products.

Mr North opened this talk by defining paint as coloured resin and proceeded to apply the doctrin of energy, ecology and economy. The ecological aspects of paint are to a large extent concerned with the elimination or reduction of solvent; the saving of energy is of paramount importance in all industrial systems. Any combination of answers to these two problems which results in economy must be of interest.

Mr North produced a chart illustrating this point.



Durability, resistance and appearance of the resulting paints, are all factors contributing to performance which must be taken into account.

If the two sides of the chart are cross referenced then the areas of interest should be highlighted.

Water-based two pack systems do exist but would seem to have a limited future. Water-based radiation cure systems seem to be of limited application.

Water-based air drying systems are used extensively as emulsion paints. Water-based low bake systems are showing steady improvement and have a good deal of scope for further development.

Powder coatings do not lend themselves to two pack systems. Radiation cured powder coating are not energy efficient as the powder must be melted prior to curing. Air drying powder coatings are not realistic. Low bake powder coatings are the most attractive area for future development, emphasising the need to decrease the melt temperatures of the polymers involved.

Solventless two pack systems, such as p.u., are already significant but there is doubtless room for expansion in this field. Solventless radiation cured systems are already regarded as a standard form. Solventless air drying systems are as old as the industry, i.e. linseed oil. An area here for development, using reactive diluents such as pentadiene acrylate, although the current limitation is the long wet time. Solventless low bake systems offer no obvious advantages.



Reader Enquiry Service No. 369

Telex 339237

occa meeting

Both hisolids and two pack air drying systems find application in maintainance coatings.

Other permutations are possible; water-based powder coatings offer certain advantages. A fine aqueous dispersion of powder reduces the dust hazard, improves the flow of the system and offers scope for low temperature curing.

Radiation cured two pack systems offer the possibility of inter-penetrating polymer networks, which is an obvious area for development.

Other areas of activity on the ecological front involve, the avoidance of formaldehyde, and developments involving a move away from acid and amine systems.

In the field of energy conservation solvent released from stoving finishes can be used to fuel the ovens, which gives scope for the use of larger quantities of cheaper solvents -a possible area for development and NAD resin systems.

For the future it would seem sensible to base new resin developments on renewable resources, which would indicate alkyd resins.

Other areas for development include:

• Hi solids coatings where rheology needs changing to avoid sag problems resulting from the lack of viscosity build up due to solvent loss.

- New thixatropic resins, with a gel strength which is not temperature dependent, can be blended with alkyds to give a range of properties.
- Resins suitable for use with aluminium dryers to give better exterior exposure with good clear varnishes for wood.

The vote of thanks for this most interesting lecture was offered by Mr Roy Wilkinson.

R.G. Handley

Hull Section

The British Board of Agrement – aims and objectives

The following is a report of the technical meeting which took place on 12 November 1984. The speaker, Mr L. Airey described the historical background to the British Board of Agrement (BBA) showing how it related to sister organisations in the EEC, South Africa, Australia and Canada. The connection between BBA and the British Standards organisation was also explained.

Many examples were given of areas of industrial technology in which BBA is involved, showing that the range of materials and systems for which certificates have been issued is very large and diverse indeed. Typical testing and certification costs were described for an exterior masonry paint.

continued overleaf



Reader Enquiry Service No. 309

occa meeting

In many cases, BBA Certificates may be used as an aid to marketing. Thus, today, where specifiers are inundated with new products and advertising literature on a wide range of materials, a BBA certificate indicates a certain technical standing for a product.

The presentation was followed by one of the liveliest discussions heard at the Hull Section for some time. By the end of the evening, everyone had a much clearer understanding of the function of BBA.

The vote of thanks was proposed by Dr N. Reeves. The meeting was attended by 18 members and guests.

P.A. Bentley

new/

New ICI Organic Division sales headquarters

The opening of the new UK sales headquarters of this division at Bolton marks further integration of the colours business of PCUK of France with ICI. The Bolton complex is a modern purpose built building, formerly the Alliance Dye & Chemical headquarters, the selling arm of PCUK in Britain, which was built in 1981.

Before outlining the changing pattern in the colour consuming industries, Jim Keaton the marketing director introduced the highly experienced sales team; most of whom had international experience. The acquisition of PCUK in 1982 had doubled the ICI colours product range to nearly 3,000 dyes, pigments, and colour auxiliaries and the new organisation will combine the sales activity of ICI Blackley and ADC, backed by first rate modern technical service facilities.

In a very comprehensive survey of the changing climate in the colour user industries covering textiles, surface coatings including inks and plastics it was pointed out that the large scale business in these areas was dominated internationally by Europeans. The six major companies were ICI, and three German and two Swiss companies, all of whom manufacture in other countries including the USA and the Far East.

The general manager Peter Macdonald in outlining the re-organisation stated that it was their aim to restructure the colours business more closely around the needs of the customer; to focus strongly on customer philosophy, and to give a useful selling structure which will satisfy customers and set ICI apart from other suppliers.

By computerising all internal ordering and despatch functions it is possible to transmit



all the orders received to the despatch warehouse at Heywood within one minute, then to finalize all the required paperwork in three minutes. At present from 1,318 customers they receive 50,000 orders per year and despatch 70 tons of material each day from Heywood. This capacity will be increased in 1985, still however with the same main object, which is: to deliver what you want, where you want it, and when you want it at the most economical price.

The assistant sales manager Richard Walsham then supervised a tour of the very well appointed laboratories, introducing the technical staff in charge. A short and interesting survey of the range of new products was given by Roy Falden and Eric Hartley, who with Richard Walsham are well known members of the Manchester Section.

In conclusion, it was a very efficient and highly informative excursion to a company that have never rested on their laurels, but have continued producing new products in a highly sophisticated competitive field, whilst at the same time still focussing on the needs of our very complex industry. It all seems a far cry from my early days, when monastral blue was bought in 7 lb tins, and kept in the chief chemist's office to be weighed out with a tablespoon as required.

N. H. Seymor

No go in the USA, but in Europe maybe

NL Industries, Inc. have announced that they would not pursue their acquisition of American Cyanamid's titanium dioxide pigment business because the Federal Trade Commission voted, with chairman Miller dissenting, to file a suit challenging the transaction. When the proposed acquisition was announced in October 1984 NL indicated it would consider expanding the American Cynamid titanium dioxide plant located in Savannah, Georgia, USA. NL now plans to increase its own capacity, using NL's proprietary chloride process technology. Sites being considered by NL for expansion are its titanium dioxide plants in Canada and Europe. Fred Montanari, executive vice-president of NL Industries and president of NL Chemicals, stated: "NL is disappointed that the proposed acquisition will not occur. Despite the FTC decision, NL remains fully committed to the titanium dioxide pigment business and intends to expand its capacity to supply the needs of titanium dioxide customers".

Reader Enquiry Service No. 31

new/

BP subsidiary closes down

Bakelite UK Ltd, a wholiy owned subsidiary of BP Chemicals Ltd, has ceased manufacture. Closure resulted in the loss of some 350 jobs at the Tyseley, Birmingham site.

Continuity of supply of some products will be ensured by licensing the formulations of certain moulding materials for manufacture by Vynckier of Belgium, a wholly owned subsidiary of GEC, and certain FR2 VO copper clad phenolic paper laminates for manufacture by Dynamit Nobel. The market will be supplied through the UK Marketing Groups of the two companies.

BP Chemicals Ltd acquired Bakelite UK Ltd in 1977. It was then the Thermosetting Division of Bakelite Xylonite Ltd, producing phenolic resins, moulding materials and industrial laminates. The phenolic resins business was transferred to BP Chemicals, Barry Division. in 1983.

Considerable overcapacity in moulding materials in Europe has resulted in severe competition from cheaper imported material with the result that Bakelite had been unable to get an economic price for its products. *Reader Enquiry Service No. 32*

ICI appoints new 'Fluon' distributor

Lawter International Ltd has been appointed UK distributor for small quantities (maximum 200 kg per order) of 'Fluon' PTFE lubricant powder grades from ICI,

In this positive move to expand a growing area, the combination of ICI's technical resources and Lawter's specialised expertise in supplying synthetic resins, printing ink vehicles and other materials to the coatings industry will, it is claimed, both improve the service offered to 'Fluon' users and extend the range of materials available from Lawter. *Reader Enguiry Service No. 33*

Chemical distribution appointment

The UK's largest chemical distributor, Ellis & Everard (Chemicals) Ltd, has been appointed to handle selected products from the Bevaloid range of chemicals used in the control of industrial processes.

These products include non-silicone defoaming agents, dispersing agents and other performance chemicals with wide applications throughout chemical process industries.

Bevaloid defoamers control foam during the production and use of paints and adhesives, the production of paper, in textile dyeing and other manufacturing processes in which foam reduces plant capacity or damages final product quality. Bevaloid dispersants have numerous applications with clays, pigments and fillers, including the The Bevaloid range will complement existing products supplied by Ellis & Everard, particularly to the paint industry, including silicone defoamers, hypochlorite, formic acids and a range of bleaches.

Bevaloid, a member of RTZ Chemicals, is based at Beverley, Humberside, and specialises in solving industrial processing problems including foam control, slurry dispersion and water hardness control. *Reader Enguiry Service No. 34*



The refurbished Miles Messenger

Valentine helps revive World War II plane

Valentine has supplied the paint and technical support to refinish one of only two remaining World War II Miles Messenger aeroplanes. This plane had been grounded for seven years, during which time, the Bristol Plane Preservation Unit decided to restore it and make it airworthy. Eighty-one Miles Messengers were built between 1943 and 1950; twenty of which were used by the RAF during the war.

Capable of flying at speeds as low as 30 mph, the Messenger was a useful aircraft for observation and reconaissance. Its ability to take-off and land in short, confined spaces added to its usefulness, and made the Messenger Field Marshall Montgomery's preferred aircraft just after D-day. It was used by Monty and his staff until the end of the war.

Reader Enquiry Service No. 35



Pneumatic Test Panel Spray System

A pneumatically operated, automatic test panel spraying unit which is said to be ideally suited for use in hazardous locations is now available. The SFS model 1000/01 from Spray Finishing Systems Ltd is British designed and is claimed to cost less that half



SFS's new test panel spraying unit

that of comparable, electro-mechanical equipment.

While special requirements can be accommodated, standard units spray a panel area of 610 mm (24 in) wide by 457 mm (18 in) high can be operated fully automatically or manually overriden. They suit a wide variety of applications in research and development, routine sampling, batch testing and colour matching.

Pneumatic operation of the model 1000/01 means a lighter weight unit that can be manoeuvred through standard door apertures, and the wheeled carriage and controls are encased within a stainless steel cover for protection and ease of cleaning.

In use automatic or cup spray guns can be mounted and an actuating cylinder is provided to operate the trigger of a manual gun. Quick adjustment is provided for spray distance and traverse speed. Dwell time between strokes may be set between two to 30 seconds and the number of coats selected between one and 99. Only a 7 bar dry air supply is required.

Reader Enquiry Service No. 36

Anionic Dispersant for Emulsion Paints

Tambour Ltd (Israel) has, for the past year, been using its own dispersant (Disperse-One) in the manufacture of its emulsion paints. Disperse-One was developed in Tambour's R & D laboratory since it was felt that money could be saved by making its own pigment dispersant.

The new product is said to be more efficient than most of the dispersants found on the European and North American Markets.

Disperse-One is also said to be substantially cheaper that other dispersants and its

new/

manufacture to be simple and straightforward. It is synthesized from readily available raw materials; the process being carried out batchwise, in any common resin kettle, and under atmospheric pressure.

Typical product data are:

Туре	Polycarboxylic
Counter-ion	Na +
Non-volatiles (%)	44-46
Ph (at 1% concentration)	0.5-2.0
Appearance	Amber liquid (slightly hazy)

Reader Enquiry Service No. 37

Fluorescence

Glen Creston have introduced a total of nine different Spectrofluorometer systems which make up the SPEX FLUOROLOG-2 series. Each is controlled by the new DMIB Spectrocopy Laboratory Coordinator.

Research grade performance is said to be provided by all the nine instruments but one has the opportunity of selecting the most suitable instrument for one's application as Glen Creston offer the choice of single or double spectrometers, 150 or 450W Xe lamps, and cooled or uncooled detectors. A wide range of accessories for polarization, phosphorescence and kinetics experiments are also available, and photon counting is standard for all systems.



The SPEX FLUORLOG-2 from Glen Creston

New catalogues on the FLUORLOG-2 and DM1B Spectroscopy Laboratory Coordinator are now available. *Reader Enguiry Service No. 38*



Mr David Winterbottom has been appointed group deputy chief executive of Evode Group plc. Mr Winterbottom will continue to be responsible for the Paints and Plastics Division. In addition, the managing directors of the Adhesives and Sealants Division at the Roofing and Insulation Division will report to him in his new senior role.



Dr K. G. Seifert, director of Hoechst AG's Zentrale Direktionsabteilung, has been elected as a non-executive director to the board of Hoechst UK, the British subsidiary of Hoechst AG, one of the world's largest chemical companies.



Dr K. G. Seifert



bri newr

British Standards

The publications listed below are new and revised British Standards. An existing BSI publication bearing a number identical to one announced below is automatically withdrawn. In all other cases of supersession, details are given in the appropriate announcement and a corresponding entry appears in the "Standards withdrawn" section.

BS 3900:

Methods of test for paints

BS 3900: Part A10: 1985 =ISO 3233 Determination of volume of dry coating (non-volatile matter) obtained from a given volume of liquid coating.

Describes the procedure for evaluating the non-volatile matter in paints. (See also BS 3900: Part B2.) Supersedes BS 3900: Part A10: 1976.

8 page Gr 5

BS 3900: Part F12: 1985 ≡ISO 7253 Determination of resistance to neutral salt spray.

Describes a procedure for evaluation corrosion resistance of paint films. (See also BS 3900: Part F4.) No current standard is superseded. 6 page Gr 4

BS 4359:

Determination of the specific surface area of powders.

BS 4359: Part 1: 1984 Recommended gas adsorption (BET) methods

Recommends three methods, plus the necessary outgassing, for determining the specific surface of a powder by measuring the quantity of gas which would cover the surface with a single layer of adsorbed gas molecules. Supersedes BS 4359: Part 1: 1969.

28 page Gr 7

Amendments

3262: 1976 Specification for hot applied thermoplastic road marking materials. Amendment No. 4 Gr 2 AMD 4754

Special Announcements

EN 53: 1974 Paints and varnishes. Determination of the danger classification by flashpoint (closed-cup method)

The above European Standard reproduced, with some modifications, the text of ISO 1516: 1973. It was implemented as a dualnumbered British Standard as BS 3900: Part A8: 1976. Since then, ISO 1516 has been revised by ISO/TC 35 and the second edition was published in 1981. CEN has now decided to withdraw EN 53: 1974 as this new edition of the International Standard is a satisfactory equivalent. Accordingly, ISO 1516: 1981 will be implemented as a revision of BS 3900: Part A8. This new edition will be published in 1985.

Proposals for withdrawal

244 & 290: 1962 Turpentine for paints Obsolete

Standards withdrawn

4699: 1971 PTC/12 Method for determination of specific gravity and density of petroleum products (graduated bicapillary pyknometer method) Superseded by BS 4699: 1985

5093: 1974 PTC/1 Method for the determination of relative density and density of petroleum products by the capillary-stoppered pyknometer method Superseded by BS 4699: 1985

New ISO Standards

ISO 4618:

Paints and varnishes – Vocabulary ISO 4618/2: 1984 Terminology relating to initial defects and to undesirable changes in films during ageing 18 page K ISO 4618/3: 1984 Terminology of resins 9 page F

beiter	Unmistakably better – cross-hatch adhesion test comparison proves it. Paints and lacquers with only small additions of Adhesion Resin LTH (solid) or Adhesion Resin LTW (liquid), apart from good light and weather resistance, attain significantly en- hanced adhesion to metal and mineral substrates, and also to plastics.
	Find out more about our new devel- opment, Adhesion Resin BL 305.
	hists (U.K.) Ltd., Central Court, 1b Knoll Rise, Orpington, Kent BR6 OJA
	Please tell me more about Adhesion Resins LTH/LTW Newly developed Adhesion Resin BL 305
	Name
	Position
	Company
	Address
	Telephone
	CHEMISCHE WERKE HÜLS AG

OCCA Conference 1985 – New substrates, new materials, new problems?

As already announced the Association's Biennial Conference will take place in Edinburgh 26-29 June 1985. Twenty-three papers on the theme will be presented in four sessions in the mornings and afternoons of Thursday 27 June and Friday 28 June. Details of both the technical programme and the social programme were given in the registration form, a copy of which was enclosed with each issue of the February *JOCCA*. In addition the technical programme appeared on page 53. Further copies can be obtained from Priory House; photostats of the registration form will be acceptable but all applications must be accompanied by the appropriate remittance.

Accommodation is being held for the Association until 1 April for delegates at both the Dragonara and Grosvenor Hotels and the Pollock Halls of Residence, although every attempt will be made to find accommodation for delegates after that date. Expotel are also holding a limited number of rooms and the Association has booklets on alternative accommodation for delegates wishing to make their own arrangements.

The social programme is a very full one in honour of the 50th Anniversary of the formation of the Scottish Section. It includes a special entertainment by that Section, coach tours to places of interest, a Jacobean banquet, a reception for overseas visitors and the Association Dinner Dance on the Friday evening, together with a golf tournament for the Sam Sharp OCCA Conference Golf Trophy.

Further summaries of papers and biographies of authors

Performance of a novel corrosion inhibiting pigment of low toxicity, in ferrous metal primers, applied to marginally prepared surfaces

P. A. Draper

Summary

The new ferro-organic pigment shows promise as a non-toxic replacement for conventional anti-corrosive pigments. Details of laboratory evaluation by means of accelerated testing of the pigment are presented. The protection afforded to abrasive blast cleaned steel is compared to that of wire brushed, previously rusted steel. In addition, the results of a limited amount of outdoor exposure are discussed. The pigment has been useful in both epoxy and alkyd binders and the paper deals with the experimental work carried out to produce starting formulations of primers in these mediums which have performance at least equal to those based on pigments such as red lead, zinc chromate and zinc phosphate. A tentative theory for the mechanism of the corrosion inhibition is also advanced.

Biography

Mr P. A. Draper obtained his BSc in 1960 with majors in Chemistry and Physics. He also has a diploma in management and administration.

From 1955 to 1959 he worked as a laboratory assistant with African Bitumen Emulsions (Pty) Ltd. In 1960 he became their chief chemist and during this period their complete epoxy product range was developed as original work in their Durban laboratories. This included a range of anticorrosion coatings, concrete protection wall, floor coatings and powder coatings.

In 1969 he co-founded a company specializing in the manufacture and application of specialist construction resins and surface coatings, and served as technical director until 1981.



P. A. Draper

Since then he has established a consultancy practice in the field of surface coatings and construction resins. In this capacity he is responsible for specification writing, QA/QC and problem solving in the coating industry. A project led by the consultancy is the subject of the paper i.e. the evaluation of the new pigment in order to assess its commercial potential.

Mr Draper has been a member of OCCA since 1959 and was admitted as a Fellow in 1981. He is alo a member of the S.A. Corrosion Institute, the National Association of Corrosion Engineers (NACE) and the South African Society for Quality Control.

Novel corrosion inhibitors

Z. Kalewicz

Summary

The necessary role of primer in any coating

system used for corrosion protection of iron and steel is well recognized.

The so-called zinc-rich primers, which are highly loaded with metallic zinc (zinc dust) present some disadvantages associated with their application: high cost, poor weldability, and a tendency to blister when exposed to aggressive, industrial atmospheres.

The paper describes the composite zinccontaining pigment composed of an electrically conducting nucleus surrounded by particles of metal zinc. This pigment behaves anodically to all corrodible steels and thus protects them from electrochemical corrosion. Di-iron phosphide has been used as the material for nuclei of this inhibitor pigment. The metal zinc deposited around the particles of di-iron phosphide diffused inside resulting in the formation of composite pigment particles; each particle constituted of an electrically conducting nucleus, a diffused interface and finely dispersed particles of zinc. The results of both short-term accelerated tests (salt-spray and humidity) and on natural weathering are given. The mechanism by which these inhibitors are believed to operate in paint film is described and the advantages of technology and application are discussed.

Biography

A native of Kielce, Poland, Mr Z. Kalewicz is the chief engineer in the R & D laboratories of Derivery Ltd Co., France.

Mr Kalewicz holds a BS degree in physical chemistry from Jagiellonian University of Cracow.

After the research works on furfuryl alcohol resins, he received his MS degree from the Institute of High Polymers Chemistry in Warsaw and joined the Institute of Precision Mechanics. Warsaw, as a senior group leader in the organic coatings laboratories.

Mr Z. Kalewicz has three patents to his name and has authored more than 30

occa conference

technical papers, most of them dealing with anticorrosion aspects of coatings technology. He is a member of OCCA, with the professional grade of FTSC, and is a member of the National Association of Corrosion Engineers.



Z. Kalewicz

New developments in selfpolishing antifoulings

C. M. Sghibartz

Summary

Since their introduction in the early seventies, selfpolishing antifouling paints have steadily increased their share of the market at the expense of the old, long life , antifoulings.

This paper deals with the latest developments in this interesting and competitive field.

Biography

Dr C. M. Sghibartz studied Chemistry at Imperial College, London, graduating with



C. M. Sghibartz

BSc (Honours) in 1974. He continued his studies at King's College, London, completing his doctorate in 1977.

He was then employed by International Paint, Felling, England, where he worked for five years.

Dr Sghibartz joined Jotun Marine Coatings over two years ago in the capacity of research and development manager, antifoulings.

Author of numerous papers, patents and articles on antifouling paints, Dr Sghibartz is spokesman on technical matters for Jotun Marine Coatings worldwide.

Colouration of UV Curing Systems

V. Kaden and P. Eckert

Summary

Based on practical work, a general overview of possibilities to colour UV systems is presented. The following groups of materials are considered:

- Organic powder pigments
- Special preparations
- Solvents soluble dyes

For each of these groups their influence on for example, the choice of resin, the dispersion process, storage stability as well as other applicational properties are discussed and comparisons with conventional systems presented.

Biography

Born in 1932 in Basle, Mr P. Eckert studied chemistry at the ETH in Zürich and textile chemistry at the Institute of Technology in Winterthur (Switzerland). He joined Ciba at Basle, Switzerland in 1958 as a chemist at the Pigment Research Department.

From 1960 he held various responsibilities in the Pigment and Dyestuff Application Department in paints, inks and allied fields. From 1970 until 1981 he was head of the Ink Application Group of Ciba-Geigy, Basle, and from 1982 until 1984 he was department head of Application and Quality Control at Ciba-Geigy Pigments, Paisley, Scotland.

Since 1984 Mr P. Eckert has been responsible for the Paint and Ink Industry and Application of Ciba-Geigy Pigment Section, Switzerland.

Born in 1938 in Germany, Dr V. Kaden was educated at the Technical University of Berlin and the Technical University of Stuttgart. He gained a PhD from "Forschungsinstitut fur Pigmente und Lacke e.V." on "Surface Phenomenon on Pigment Surfaces".



P. Eckert



Dr V. Kaden

Since joining Ciba-Geigy, Basle, in 1968 Dr Kaden has been involved with a wide variety of technical activities associated with the pigments and dyestuffs business, often in close collaboration with the R & D functions. His main fields of activities have been in the printing ink and paint sectors where he has made a special study of the dispersion process. Previous papers published have been on the adsorption and desorption of macromolecules and more recently (FATIPEC, Budapest 1978) on the dispersion of pigments. He serves as a committee member of a DIN working party on test methods and is a member of the "Schweizerischen Vereinigung der Lack-und Farbenchemiker".

At present Dr Kaden is on secondment to Ciba-Geigy, Paisley, where he is involved with the setting up of the international technical service function.

occa new/

Eastern Branch

Annual skittles match

The Annual Skittles Match was held at the Murrayfield Indoor Sports Centre, Edinburgh on Friday 19 October 1984 where the Newton Cup was retrieved by the West of Scotland Captained by Dr S. G. Lawrence with a score of 1,860 points against a total of 1,796 points obtained by the East of Scotland team captained by Nigel Baird. The full results were as follows:

Individual Prizes

1st Lady		
Louise Kirkwood	West	160 points
2nd Lady		
Lyn Robertson	East	154 points
3rd Lady		100
Jacqueline Henderson	west	150 points
Boody	West	02 noints
Ann Flood	west	85 points
1st Gent		
Alan Baird	West	231 points
2nd Gent		
Denis Gibson	West	218 points
3rd Gent		212
Volker Kaden	West	212 points
Booby		127
Gunther Wuchner	west	13/points

It seems reasonably clear that the West were successful in retrieving the trophy by packing their side with visiting stars namely Volker Kaden and Gunther Wuchner from Skittle Clubs Basle and Wehr respectively. It remains to be seen what the reaction of the East will be next year.

A very enjoyable night was had by all. The organisers would like to thank the following for donating prizes: R. G. Gardiner (Alexander G. Paterson Ltd), A. Gibson (Alexander Fergusson & Co), A. Hunter (Samuel Banner), W. Jack (Tioxide UK Ltd), A. McKendrick (Craig & Rose PLC), J. Wilson (Ciba Geigy PLC) and Esso Chemicals.

Dr J. H. Coy

Obituaries

F. D. H. Sharp

It is with regret that we record the death on Tuesday 5 February 1985 of Mr F. D. H. Sharp (Chairman of the London Section and a former Chairman of the Irish Section) at the age of 50. The funeral took place on 13 February and was attended by many of his colleagues as well as representatives from the Association, the London Section, and other Sections.

The following tributes have been received:

N.A. McInerney writes:

It was with a great sense of shock and much sadness that we learned of the sudden death of our Past Chairman and friend Mr David



F. D. H. Sharp

Sharp. His widow Barbara and family have requested friends to give a donation to the British Diabetic Association instead of sending flowers.

David's departure leaves a void that will never be filled. He leaves an unforgettable memory with us of a talented man who had many different qualities to suit whatever job he had in hand, whether it was as top salesman or OCCA function organiser. His loyalty to his company, his kindness and his ever present sense of humour were renowned. "Ar dheis De go raibh a anam" – an Irish prayer used at a sad time such as this which wishes David happiness and peace with God.

J. D. Sanders writes:

David and I first met in 1952 when we were both teenagers and he was an assistant in the wool laboratory at Bradford. Even in those days he was larger than life and there was a constant flow of backchat with anyone who happened to come within earshot. He had joined Geigy from Giggleswick School where he had been a boarder and had excelled himself at rugby and cricket.

In course of time he became a representative and moved to Ireland. He transferred from dyestuffs to pigments and after a number of years returned to the UK, finally moving from Scotland to the London area in 1978. During this time David accumulated an astonishingly wide circle of friends and acquaintances. There was nothing calculated or self-interested in this – he just enjoyed people.

He was devoted to OCCA, becoming Chairman of the Irish Section in the mid-60s and was a member of Council for many years. At the time of his death he was Chairman of London Section.

Stories about David abound. On one occasion when David was visiting Paisley from Ireland he was taken to hospital with a

diabetic attack. A colleague called on him and expected him to be horizontal and comatose. Far from it – there he was, large as life, reading out jokes from *Playboy*, with nursing staff and patients in stitches.

On another occasion I remember travelling with a number of colleagues from Glasgow to Manchester by air one wintry evening. Fog descended and we were waiting silently in the coach with 20 or 30 other people ready to move off to Prestwick. David must have heard what was going on as he suddenly appeared, picked up the driver's hat from his seat and made as if to drive us away. He kept the whole coach in hysterics for 15 minutes, when he vanished as quickly as he had come.

Devoted as he was to his family one felt at times that he would willingly have spent all his waking hours, and that was most of them, in the company of his customers. It could certainly be hard to keep up with him. He met me one evening at Watford station and we called for a quick one at some little place he had recently discovered. Sure enough a customer appeared – not even one of his – and we were still at it at the customer's home at 2 am David collected me from my hotel at 6.45 am and in the course of some 300 miles we made three customer visits and had dinner with one of them afterwards in the wilds of Essex, another 2 am finish. It took me a fortnight to recover, but there was Sharpie bright and cheerful on the phone next day to see if I had got back safely

David's friends and colleagues will remember him as a spontaneous, endearing, unpretentious person. He was never afraid to speak his mind and did not suffer fools gladly. He was a true professional. His zest for life, his love of people and his enthusiasm for his job were without parallel. We shall all miss him greatly.

D. H. W. Lovegrove

H. J. Clarke writes:

It is with much sorrow that we record the death of David Lovegrove who died on 30 January 1985 at the age of 52.

David who joined Carrs Paints Ltd in 1948 was a much loved and respected member of the Midlands Paint Industry. He joined OCCA and the Birmingham Paint Varnish, Lacquer Club in 1962 (He was president of the latter in 1972-73 and Society Representative to its Federation in the States since 1975).

He contributed much to the Industry and was always a very happy friend to many people, not only in the Paint Industry but also to many users of paint. His hobby was gardening, about which he would always offer advice when asked. He will be sadly missed.

David is survived by his wife Margaret, his two daughters Karen and Sara, and son Robert. I-RAW MATERIALS AND THEIR USA

Prepared by OCCA Australia

As a consequence of the comments and criticisms of the first edition of "Surface Coatings" (1974), it was decided to produce a second edition with a different approach. While it has again been designed to serve as a guide and a reference document for students, it is also intended to provide an up-to-date, in-depth treatment of all relevant areas of paint technology.

The work is presented in two volumes, the first extensively reviewing the raw materials used in surface coatings, and the second the technology of the products that use them. Volume 1 will also be of considerable benefit to students, technologists and others in related industries such as inks, adhesives, ceramics, textiles and cosmetics, and raw material suppliers. It provides an excellent introduction to polymer science, pigments, solvents and additives. This edition reflects the movement towards aqueous systems: the chapters on alkyds have been reduced in this edition from six to three, and the four solvent chapters combined. Conversely the emulsion chapters have been doubled to six, and three new chapters on aqueous resins added. Volume 2, whilst retaining the basic manufacture. application and technology coverage, is based on completely updated contributions. There are additional chapters on lacquers, powder coatings, UV-cured coatings and decorative paint selection. Reflecting the increasing impact of computers, there are new chapters on automated colour matching and applications in resin and coating formulation.

Volume 1 is available by placing orders (prepayment only) through the Oil & Colour Chemists' Association at $\pounds 27.50$ (inc. p&p in the UK) plus $\pounds 2.50$ for orders sent overseas by surface mail.

Volume 1 - Hardback - 408 pp.

Contents

The Past, Present and Future of the Surface Coatings Industry Introduction to Polymer Science Vegetable Oils Oleoresinous Media Alkyd Resin Technology Manufacture of Alkyd Resins Applications of Alkyd Resins Polyesters Amino Resins Phenolic Resins Polyurethane Resins **Epoxy Resins** Water Dispersible Epoxy Coatings Silicone Resins Acrylic Solution Resins Emulsion Polymerization Theory **Emulsion Properties 1:** Effect of Monomer Composition **Emulsion Properties 2:** Effect of Water Phase and Particle Size **Emulsion Properties 3:** Film Formation Emulsion Polymers: Manufacture and Testing Applications of Emulsion Polymers Water-Reducible Resins _____

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G Graco UK Ltd	(369)	76
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M		
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NI Chemicals (UK) I td	(367)	i
R	(202)	
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